In the Claims:

Please amend the claims as follows:

 (Currently amended) A process for production of higher linear alpha olefins and/or alkyl-branched alpha olefins <u>having a chain length of from 4 to 100 carbon atoms</u> comprising:

co-oligomerising one or more alpha olefins other than ethylene with ethylene in the presence of a metal catalyst system employing one or more bis-aryliminepyridine MX_a complexes and/or one or more [bis-aryliminepyridine $MY_p.L_b^+$][NC $^-$] $_q$ complexes, said bisaryliminepyridine complexes comprising a ligand of the formula,

$$R_{4}$$
 R_{2}
 R_{3}
 R_{5}
 R_{5}
 R_{1}
 R_{2}
 R_{3}
 R_{5}
 R_{5}

wherein M is a metal atom selected from Fe or Co; a is 2 or 3; X is halide, optionally substituted hydrocarbyl, alkoxide, amide, or hydride; Y is a ligand which may insert an olefin; NC- is a non-coordinating anion; p+q is 2 or 3, matching the formal oxidation of said metal atom; L is a neutral Lewis donor molecule; b = 0, 1, or 2; R_1 - R_5 are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 vicinal to one another taken together may form a ring; each Z, which may be identical or different, is an optionally substituted aromatic hydrocarbon ring; an optionally substituted polyaromatic hydrocarbon moiety; an optionally substituted heterohydrocarbyl moiety; or an optionally substituted aromatic hydrocarbon ring in combination with a metal, said optionally substituted aromatic hydrocarbon ring being π -co-ordinated to the metal; said co-oligomerising being carried out under conditions comprising an ethylene pressure of less than 2.5 MPa from about 0.1 MPa to about 1.6 MPa and a temperature of from about -100°C to about 300°C.

2. (Original) The process of Claim 1 wherein said ligand is of the formula,

$$\begin{array}{c|c} R_1 & R_3 \\ \hline R_4 & N & N \\ \hline R_7 & R_8 & R_{10} \\ \hline R_8 & R_{10} & R_{10} \\ \hline \end{array}$$

(II)

wherein R_1 - R_{10} are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 , R_6 - R_{10} vicinal to one another taken together may form a ring; R_6 may be taken together with R_4 to form a ring; R_{10} may be taken together with R_4 to form a ring; Z is an optionally substituted aromatic hydrocarbon ring; an optionally substituted polyaromatic hydrocarbon moiety; an optionally substituted heterohydrocarbyl moiety; or an optionally substituted aromatic hydrocarbon ring in combination with a metal, said optionally substituted aromatic hydrocarbon ring being π -co-ordinated to the metal.

3. (Original) The process of Claim 1 wherein said ligand is of the formula,

wherein R_1 - R_5 , R_7 - R_9 and R_{12} - R_{14} are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 , R_7 - R_9 and R_{12} - R_{14} vicinal to one another taken together may form a ring; R_6 is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_7 or R_4 to form a ring; R_{10} is hydrogen, optionally

substituted hydrocarbyl, an inert functional group, or taken together with R_9 or R_4 to form a ring; R_{11} is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_5 or R_{12} to form a ring; and R_{15} is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_5 or R_{14} to form a ring.

4. (Original) The process of Claim 3 wherein R_1 - R_5 , R_7 - R_9 and R_{12} - R_{14} are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 , R_7 - R_9 and R_{12} - R_{14} vicinal to one another taken together may form a ring; R_6 is a primary carbon group, a secondary carbon group or a tertiary carbon group; and provided that:

when R_6 is a primary carbon group none, one or two of R_{10} , R_{11} and R_{15} are primary carbon groups, and the remainder of R_{10} , R_{11} and R_{15} are hydrogen;

when R_6 is a secondary carbon group none or one of R_{10} , R_{11} and R_{15} is a primary carbon group or a secondary carbon group and the remainder of R_{10} , R_{11} and R_{15} are hydrogen;

when R_6 is a tertiary carbon group all of R_{10} , R_{11} and R_{15} are hydrogen; and any two of R_6 , R_7 , R_8 , R_9 , R_{10} , R_{11} , R_{12} , R_{13} , R_{14} and R_{15} vicinal to one another, taken together may form a ring.

- 5. (Original) The process of Claim 3 wherein R_1 - R_5 , R_7 - R_9 and R_{12} - R_{14} are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 , R_7 - R_9 and R_{12} - R_{14} vicinal to one another taken together may form a ring; R_6 is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_7 or R_4 to form a ring; R_{10} is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_9 or R_4 to form a ring; R_{11} and R_{15} are, independently, hydrogen or an inert functional group.
- 6. (Original) The process of Claim 3 wherein R_1 - R_5 , R_7 - R_9 and R_{12} - R_{14} are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 , R_7 - R_9 and R_{12} - R_{14} vicinal to one another taken together may form a ring; R_6 , R_{10} , R_{11} and R_{15} are identical and are each selected from fluorine or chlorine.
- 7. (Currently amended) A process for producing higher linear alpha olefins and/or alkyl-branched alpha olefins <u>having a chain length of from 4 to 100 carbon atoms</u> comprising:
- co-oligomerising one or more alpha olefins other than ethylene with ethylene in the presence of a metal catalyst system employing one or more bis-aryliminepyridine MX_a complexes and/or one or more [bis-aryliminepyridine MY_p.L_b+][NC]_q complexes, said bis-aryliminepyridine complexes comprising a ligand of the formula,

$$R_4$$
 R_2
 R_3
 R_5
 R_5
 R_7
 R_8
 R_9
 R_9
 R_9

wherein M is a metal atom selected from Fe or Co; a is 2 or 3; X is halide, optionally substituted hydrocarbyl, alkoxide, amide, or hydride; Y is a ligand which may insert an olefin; NC is a non-coordinating anion; p+q is 2 or 3, matching the formal oxidation of said metal atom; L is a neutral Lewis donor molecule; b = 0, 1, or 2; R₁-R₅ are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R₁-R₃ vicinal to one another taken together may form a ring; each Z, which may be identical or different, is an optionally substituted aromatic hydrocarbon ring; an optionally substituted heterohydrocarbyl moiety; or an optionally substituted aromatic hydrocarbon ring in combination with a metal, said optionally substituted aromatic hydrocarbon ring being π-co-ordinated to the metal; said co-oligomerizing being carried out under conditions comprising an ethylene pressure of less than 2.5 MPa from about 0.1 MPa to about 1.6 MPa and a temperature of about -100°C to about 300°C, wherein alpha olefin co-monomer is present in a concentration of greater than 1 mol.Γ¹.

Claims 8-12 (Canceled).

Claims 13-16 (Withdrawn)

Please amend the following new claims which were submitted in the previous paper:

4317. (Currently Amended) The process of claim 7 wherein said ligand is of the formula,

$$\begin{array}{c|c} R_1 \\ R_2 \\ R_3 \\ R_7 \\ R_8 \\ R_{9} \end{array}$$

(II)

wherein R_1 - R_{10} are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 , R_6 - R_{10} vicinal to one another taken together may form a ring; R_6 may be taken together with R_4 to form a ring; R_{10} may be taken together with R_4 to form a ring; Z is an optionally substituted aromatic hydrocarbon ring; an optionally substituted polyaromatic hydrocarbon moiety; an optionally substituted heterohydrocarbyl moiety; or an optionally substituted aromatic hydrocarbon ring in combination with a metal, said optionally substituted aromatic hydrocarbon ring being π -co-ordinated to the metal.

1418. (Currently Amended) The process of claim 7 wherein said ligand is of the . formula,

wherein R₁-R₅, R₇-R₉ and R₁₂-R₁₄ are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R₁-R₃, R₇-R₉ and R₁₂-R₁₄ vicinal to one another taken together may form a ring; R₆ is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R₇ or R₄ to form a ring; R₁₀

is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_9 or R_4 to form a ring; R_{11} is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_5 or R_{12} to form a ring; and R_{15} is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_5 or R_{14} to form a ring.

 $45\underline{19}$. (Currently Amended) The process of claim $44\underline{18}$ wherein R_1 - R_5 , R_7 - R_9 and R_{12} - R_{14} are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 , R_7 - R_9 and R_{12} - R_{14} vicinal to one another taken together may form a ring; R_6 is a primary carbon group, a secondary carbon group or a tertiary carbon group; and provided that:

when R_6 is a primary carbon group none, one or two of R_{10} , R_{11} and R_{15} are primary carbon groups, and the remainder of R_{10} , R_{11} and R_{15} are hydrogen;

when R₆ is a secondary carbon group none or one of R₁₀, R₁₁ and R₁₅ is a primary carbon group or a secondary carbon group and the remainder of R₁₀, R₁₁ and R₁₅ are hydrogen; when R₆ is a tertiary carbon group all of R₁₀, R₁₁ and R₁₅ are hydrogen; and any two of R₆, R₇, R₈, R₉, R₁₀, R₁₁, R₁₂, R₁₃, R₁₄ and R₁₅ vicinal to one another, taken together may form a ring.

4620. (Currently Amended) The process of claim 4418 wherein R_1 - R_5 , R_7 - R_9 and R_{12} - R_{14} are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 , R_7 - R_9 and R_{12} - R_{14} vicinal to one another taken together may form a ring; R_6 is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_7 or R_4 to form a ring; R_{10} is hydrogen, optionally substituted hydrocarbyl, an inert functional group, or taken together with R_9 or R_4 to form a ring; R_{11} and R_{15} are, independently, hydrogen or an inert functional group.

4721. (Currently Amended) The process of claim 4418 wherein R_1 - R_5 , R_7 - R_9 and R_{12} - R_{14} are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 , R_7 - R_9 and R_{12} - R_{14} vicinal to one another taken together may form a ring; R_6 , R_{10} , R_{11} and R_{15} are identical and are each selected from fluorine or chlorine.

Cancel claim 22 which was incorrectly numbered 18.

1923. (Currently Amended) The process of claim 1 wherein said conditions comprise a temperature of from about 0°C to about 200°C.

Cancel claim 24 which was incorrectly numbered 20.

2425. (Currently Amended) The process of claim 7 wherein said conditions comprise a temperature of from about 0°C to about 200°C.

2226. (Currently Amended) The process of claim 7 wherein said conditions comprise a temperature of from about 50°C to about 150°C.

Cancel claim 27 which was incorrectly numbered 23.

2428. (Currently Amended) The process of claim 1317 wherein said conditions comprise a temperature of from about 0°C to about 200°C.

Cancel claim 29 which was incorrectly numbered 25.

2630. (Currently Amended) The process of claim 1418 wherein said conditions comprise a temperature of from about 0°C to about 200°C.

Cancel claim 31 which was incorrectly numbered 27.

2832. (Currently Amended) The process of claim 1519 wherein said conditions comprise a temperature of from about 0°C to about 200°C.

Cancel claim 33 which was incorrectly numbered 29.

3034. (Currently Amended) The process of claim 1620 wherein said conditions comprise a temperature of from about 0°C to about 200°C.

Cancel claim 35 which was incorrectly numbered 31.

- 3236. (Currently Amended) The process of claim 1721 wherein said conditions comprise a temperature of from about 0°C to about 200°C.
- 3337. (Currently Amended) The process of claim 1721 wherein said conditions comprise a temperature of from about 50°C to about 150°C.

Cancel claims 38-49 which were incorrectly numbered 34-45.

- 46<u>50</u>. (Currently Amended) The process of claim 1 wherein said alpha olefin comonomer is present at a concentration of greater than 2.5 mol.l⁻¹.
- 47<u>51</u>. (Currently Amended) The process of claim 1 wherein said alpha olefin comonomer is present at a concentration of greater than 5 mol.l⁻¹.
- 48<u>52</u>. (Currently Amended) The process of claim 2 wherein said alpha olefin comonomer is present at a concentration of greater than 2.5 mol.l⁻¹.
- 49<u>53</u>. (Currently Amended) The process of claim 2 wherein said alpha olefin comonomer is present at a concentration of greater than 5 mol.l⁻¹.
- 5054. (Currently Amended) The process of claim 3 wherein said alpha olefin co-monomer is present at a concentration of greater than 2.5 mol.l⁻¹.
- 5155. (Currently Amended) The process of claim 3 wherein said alpha olefin comonomer is present at a concentration of greater than 5 mol.l⁻¹.
- 5256. (Currently Amended) The process of claim 4 wherein said alpha olefin comonomer is present at a concentration of greater than 2.5 mol.l⁻¹.

- 53<u>57</u>. (Currently Amended) The process of claim 4 wherein said alpha olefin comonomer is present at a concentration of greater than 5 mol.l⁻¹.
- 54<u>58</u>. (Currently Amended) The process of claim 5 wherein said alpha olefin comonomer is present at a concentration of greater than 2.5 mol.l⁻¹.
- 55<u>59</u>. (Currently Amended) The process of claim 5 wherein said alpha olefin comonomer is present at a concentration of greater than 5 mol.l⁻¹.
- 56<u>60</u>. (Currently Amended) The process of claim 1 wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 5761. (Currently Amended) The process of claim 7 wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 5862. (Currently Amended) The process of claim 1317 wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 5963. (Currently Amended) The process of claim 1418 wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 6064. (Currently Amended) The process of claim 1519 wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 61<u>65</u>. (Currently Amended) The process of claim <u>1620</u> wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 6266. (Currently Amended) The process of claim 1721 wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 6367. (Currently Amended) The process of claim 2924 wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 64<u>68</u>. (Currently Amended) The process of claim <u>2327</u> wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.

- 6569. (Currently Amended) The process of claim 4650 wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 6670. (Currently Amended) The process of claim 4751 wherein said conditions comprise a temperature and pressure effective to yield a product slate with a K-factor of from about 0.40 to about 0.90.
- 6771. (Currently Amended) The process of claim 1 wherein said conditions comprise an inert solvent.
- 68<u>72</u>. (Currently Amended) The process of claim 7 wherein said conditions comprise an inert solvent.
- 6973. (Currently Amended) The process of claim 4650 wherein said conditions comprise an inert solvent.
- 7074. (Currently Amended) The process of claim 4751 wherein said conditions comprise an inert solvent.
- 71<u>75</u>. (Currently Amended) The process of claim 65<u>69</u> wherein said conditions comprise an inert solvent.
- 72<u>76</u>. (Currently Amended) The process of claim 66<u>70</u> wherein said conditions comprise an inert solvent.
- 73<u>77</u>. (Currently Amended) The process of claim 67<u>71</u> wherein said inert solvent is selected from the group consisting of alkanes, alkenes, cycloalkanes, and aromatic hydrocarbons.
- 7478. (Currently Amended) The process of claim 6872 wherein said inert solvent is selected from the group consisting of alkanes, alkenes, cycloalkanes, and aromatic hydrocarbons.
- 7579. (Currently Amended) The process of claim 6973 wherein said inert solvent is selected from the group consisting of alkanes, alkenes, cycloalkanes, and aromatic hydrocarbons.
- 7680. (Currently Amended) The process of claim 7074 wherein said inert solvent is selected from the group consisting of alkanes, alkenes, cycloalkanes, and aromatic hydrocarbons.
- 7781. (Currently Amended) The process of claim 7175 wherein said inert solvent is selected from the group consisting of alkanes, alkenes, cycloalkanes, and aromatic hydrocarbons.

- 7882. (Currently Amended) The process of claim 7276 wherein said inert solvent is selected from the group consisting of alkanes, alkenes, cycloalkanes, and aromatic hydrocarbons.
- 7983. (Currently Amended) The process of claim 6771 wherein said inert solvent is selected from the group consisting of hexane, isooctane, benzene, toluene, and xylene.
- 8084. (Currently Amended) The process of claim 6872 wherein said inert solvent is selected from the group consisting of hexane, isooctane, benzene, toluene, and xylene.
- 8185. (Currently Amended) The process of claim 6973 wherein said inert solvent is selected from the group consisting of hexane, isooctane, benzene, toluene, and xylene.
- 8286. (Currently Amended) The process of claim 7074 wherein said inert solvent is selected from the group consisting of hexane, isooctane, benzene, toluene, and xylene.
- 8387. (Currently Amended) The process of claim 7175 wherein said inert solvent is selected from the group consisting of hexane, isooctane, benzene, toluene, and xylene.
- 8488. (Currently Amended) The process of claim 7276 wherein said inert solvent is selected from the group consisting of hexane, isooctane, benzene, toluene, and xylene.
- 8589. (Currently Amended) The process of claim 1 wherein said conditions comprise the absence of air and moisture.
- 8690. (Currently Amended) The process of claim 7 wherein said conditions comprise the absence of air and moisture.

Please add the following new claims:

91. (New) A process for production of higher alkyl-branched alpha olefins having a chain length of from 4 to 100 carbon atoms and having the general structure:

$$C = C[-C-C]_n[-C]_m(R_1)-R_2$$

wherein R_1 is a methyl group; n = 0, 1, 2, etc.; m = 1; and R_2 is an optionally substituted hydrocarbyl, said process comprising:

co-oligomerising one or more alpha olefins other than ethylene with ethylene in the presence of a metal catalyst system employing one or more bis-aryliminepyridine MX_a

complexes and/or one or more [bis-aryliminepyridine MY_p.L_b⁺][NC⁻]_q complexes, said bis-aryliminepyridine complexes comprising a ligand of the formula,

$$R_4$$
 R_2
 R_3
 R_5
 R_5
 R_1
 R_2
 R_3
 R_5

wherein M is a metal atom selected from Fe or Co; a is 2 or 3; X is halide, optionally substituted hydrocarbyl, alkoxide, amide, or hydride; Y is a ligand which may insert an olefin; NC- is a non-coordinating anion; p+q is 2 or 3, matching the formal oxidation of said metal atom; L is a neutral Lewis donor molecule; b = 0, 1, or 2; R_1 - R_5 are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 vicinal to one another taken together may form a ring; each Z, which may be identical or different, is an optionally substituted aromatic hydrocarbon ring; an optionally substituted polyaromatic hydrocarbon moiety; an optionally substituted heterohydrocarbyl moiety; or an optionally substituted aromatic hydrocarbon ring being π -coordinated to the metal; said co-oligomerising being carried out under conditions comprising an ethylene pressure of from about 0.1 MPa to about 1.6 MPa.

92. (New) A process for production of higher alkyl-branched alpha olefins having a chain length of from 4 to 100 carbon atoms and having the general structure:

$$C = C[-C-C]_n(R_1)-R_2$$

wherein R_1 is an ethyl group; n = 0, 1, 2, etc.; and R_2 is an optionally substituted hydrocarbyl, said process comprising:

co-oligomerising one or more alpha olefins other than ethylene with ethylene in the presence of a metal catalyst system employing one or more bis-aryliminepyridine MX_a complexes and/or one or more [bis-aryliminepyridine $MY_p.L_b^+$][NC]_q complexes, said bisaryliminepyridine complexes comprising a ligand of the formula,

$$R_{2}$$
 R_{3}
 R_{4}
 R_{5}
 R_{5}
 R_{1}
 R_{2}
 R_{3}
 R_{5}
 R_{5}

wherein M is a metal atom selected from Fe or Co; a is 2 or 3; X is halide, optionally substituted hydrocarbyl, alkoxide, amide, or hydride; Y is a ligand which may insert an olefin; NC- is a non-coordinating anion; p+q is 2 or 3, matching the formal oxidation of said metal atom; L is a neutral Lewis donor molecule; b = 0, 1, or 2; R_1 - R_5 are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 vicinal to one another taken together may form a ring; each Z, which may be identical or different, is an optionally substituted aromatic hydrocarbon ring; an optionally substituted polyaromatic hydrocarbon moiety; an optionally substituted heterohydrocarbyl moiety; or an optionally substituted aromatic hydrocarbon ring in combination with a metal, said optionally substituted aromatic hydrocarbon ring being π -coordinated to the metal; said co-oligomerising being carried out under conditions comprising an ethylene pressure from about 0.1 MPa to about 1.6 MPa.

93. (New) A process for producing higher linear alpha olefins and/or alkylbranched alpha olefins having a chain length of from 4 to 100 carbon atoms comprising: co-oligomerising one or more alpha olefins other than ethylene with ethylene in the presence of a metal catalyst system employing one or more bis-aryliminepyridine MX_a complexes and/or one or more [bis-aryliminepyridine MY_p.L_b+][NC]_q complexes, said bisaryliminepyridine complexes comprising a ligand of the formula,

$$R_{4}$$
 R_{2}
 R_{3}
 R_{5}
 R_{5}
 R_{1}
 R_{2}
 R_{3}
 R_{5}
 R_{5}

wherein M is a metal atom selected from Fe or Co; a is 2 or 3; X is halide, optionally substituted hydrocarbyl, alkoxide, amide, or hydride; Y is a ligand which may insert an olefin; NC is a non-coordinating anion; p+q is 2 or 3, matching the formal oxidation of said metal atom; L is a neutral Lewis donor molecule; b = 0, 1, or 2; R_1 - R_5 are each, independently, hydrogen, optionally substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 vicinal to one another taken together may form a ring; each Z, which may be identical or different, is an optionally substituted aromatic hydrocarbon ring; an optionally substituted polyaromatic hydrocarbon moiety; an optionally substituted heterohydrocarbyl moiety; or an optionally substituted aromatic hydrocarbon ring in combination with a metal, said optionally substituted aromatic hydrocarbon ring being π -co-ordinated to the metal; said co-oligomerizing being carried out under conditions comprising an ethylene pressure of from about 0.1 MPa to about 1.6 MPa, wherein alpha olefin co-monomer is present in a concentration of greater than 1 mol.l⁻¹.

94. (New) A process for production of higher alkyl-branched alpha olefins having a chain length of from 1 to 100 carbon atoms and having the general structure:

$$C = C[-C-C]_0(R_1)-R_2$$

wherein R_1 is an ethyl group; n = 0, 1, 2, etc.; and R_2 is an optionally substituted hydrocarbyl, said process comprising:

co-oligomerising one or more alpha olefins other than ethylene with ethylene in the presence of a metal catalyst system employing one or more bis-aryliminepyridine MX_a complexes and/or one or more [bis-aryliminepyridine $MY_p.L_b^+$][NC]_q complexes, said bisaryliminepyridine complexes comprising a ligand of the formula,

$$R_{2}$$
 R_{3}
 R_{4}
 R_{5}
 R_{5}
 R_{1}
 R_{2}
 R_{3}
 R_{5}
 R_{5}

wherein M is a metal atom selected from Fe or Co; a is 2 or 3; X is halide, optionally substituted hydrocarbyl, alkoxide, amide, or hydride; Y is a ligand which may insert an olefin; NC- is a non-coordinating anion; p+q is 2 or 3, matching the formal oxidation of said metal atom; L is a neutral Lewis donor molecule; b = 0, 1, or 2; R_1 - R_5 are each, independently, hydrogen, optionally

substituted hydrocarbyl, an inert functional group, or any two of R_1 - R_3 vicinal to one another taken together may form a ring; each Z, which may be identical or different, is an optionally substituted aromatic hydrocarbon ring; an optionally substituted polyaromatic hydrocarbon moiety; an optionally substituted heterohydrocarbyl moiety; or an optionally substituted aromatic hydrocarbon ring in combination with a metal, said optionally substituted aromatic hydrocarbon ring being π -coordinated to the metal; said co-oligomerising being carried out under conditions comprising an ethylene pressure of from about 0.1 MPa to about 1.6 MPa.